



# The Effects of Increased Pressure on the Reaction Kinetics of Biomass Pyrolysis and Combustion

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TAPPI Conference  
October 15, 2009



# Overview

- **Purpose: Determine Effects of Increased Pressure on the reaction rates of Biomass Pyrolysis & Combustion**
- **Objective: Reduce the fixed capital costs for biofuels plants by increasing their operating pressures**
- **Advantages/Disadvantages of Increased Pressure Effects**
- **Combustion Reaction Kinetics vs. Pyrolysis Reaction Kinetics**
- **Unusual Biomass Characteristics which affect the study of pressure on combustion and pyrolysis kinetics**
- **The potential reduction in equipment sizes with currently known information**
- **Conclusions**



# Definitions

- Combustion – the reaction of oxygen with other materials, usually organic, with the evolution of light and heat, and the production of carbon dioxide and water.
- Pyrolysis – the decomposition of organic materials due to heating in the absence of oxygen
- Kinetics – the thermodynamic field which studies the rate of chemical reactions
- Aspect ratio – surface area to volume ratio of a particle undergoing combustion or pyrolysis
- Char- the 89-90% carbon structure left after evolution of lignins and other volatiles during pyrolysis; a series of ruptured and broken cellular tubes made up of the wood grain
- Half life – time it takes for  $\frac{1}{2}$  of a biomass sample to be combusted or pyrolyzed.



# Objective



- Commercial plants should be able to produce drop-in replacement biofuels in a cost range around \$ 60/bbl, assuming feedstock costs in the \$ 30-50/dry ton range
- A common cost savings technique in the oil patch and chemical industries for gas-phase systems is to raise the pressure to reduce the size of vessels and piping.
  - Vessels and piping can run 30-40% of the fixed capital investment
  - Running at 10 x atmospheric pressure, at a straightforward ratio, the volumes required drop nearly by a factor of ten. ( But wait – there's more!)
- **Reduce Fixed Capital Costs by at least 30%**



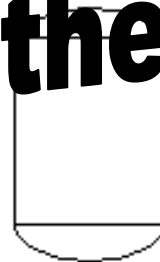
# Pressurization Advantages

- High pressure → Equipment volume reduction

**But this is only 1/2 the story....**



Vessel size at atmospheric pressure



Vessel size at 300 psig pressure

Potentially Lower Capital Cost

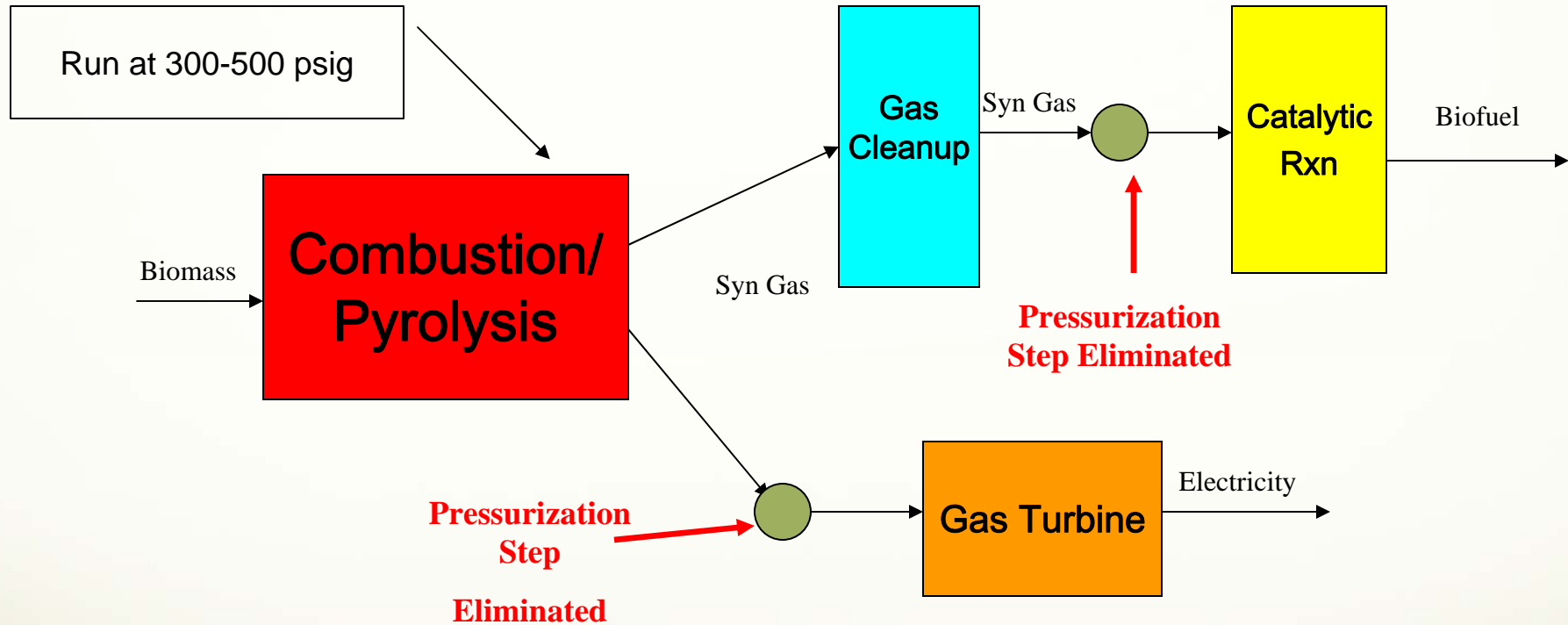


# Increased Reaction Rates also Reduce Reactor Sizes

- Reactor sizing is a function of reaction rate, residence time, and approach to equilibrium. Pyrolysis reactions do not reach equilibrium quickly in the gas phase.
- At the same pressure, a faster reaction rate requires less residence time, and thus a smaller vessel.
- Thus, a faster reaction rate resulting from increased pressure has two multiplying factors to further reduce equipment sizes:
  - Higher pressure by volume reduction
  - Lower residence times by faster reaction rates
- The combination reduces the volume by MORE than the pressure ratio.



# Another Pressurization Advantage



If combustion/pyrolysis is pressurized:

**Eliminates Costly Downstream Compression Steps**



## Hydrogen impact on compression costs

- Biomass syngases contain lots of hydrogen, anywhere from 15-50%.
- Hydrogen compressors are particularly expensive, due to the low density of hydrogen
- Hydrogen leakage from rotating equipment with seals can be a problem, and hydrogen flames are invisible in daylight
- The parasitic electrical load for compression is very high; it can run 10% of the produced electrical load.





# Other Pressurization Advantages

- Smaller equipment sizes mean smaller surface areas for thermal heat losses
- Lower thermal heat losses yield higher internal reaction temperatures
- Higher reaction temperatures favor lower tar formation levels.
- Easier gas cleanup via larger allowable pressure drops in cyclones, filters and scrubbers
- Lower tar formation at higher pressures
- More effect latent heat recovery from water condensed from syngas



# Pressurization Disadvantages

- Four main categories:
  - Mechanical Problems with equipment at elevated pressure
  - Less-than-linear reactivity increase due to pressure
  - Increased emissions
  - Possible increased methane concentrations in the syngas



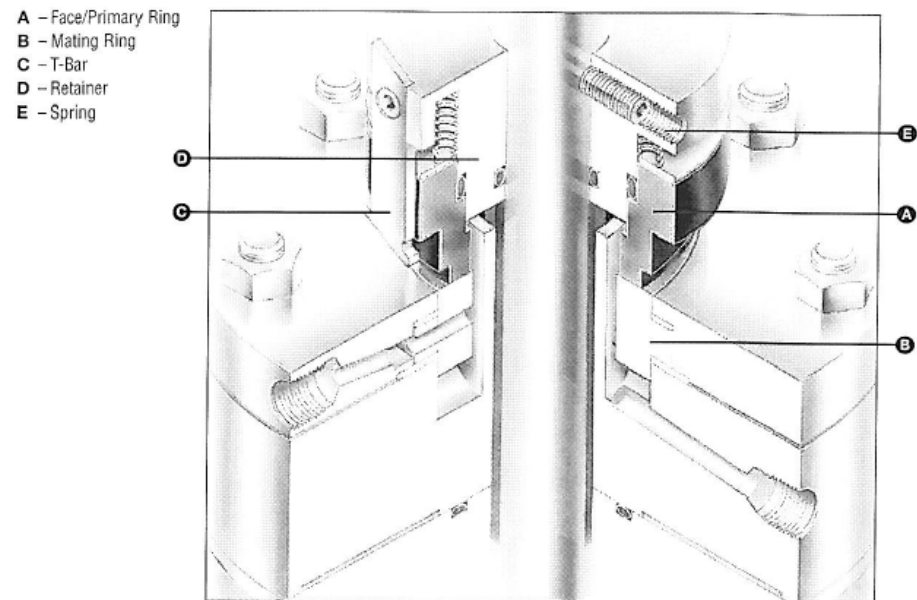
# Feed System Challenges

- Pyrolysis needs to remove the void space air between the biomass particles – backflush with nitrogen or steam needed.
- Nitrogen expensive, but steam has its problems:
  - Terpenes in biomass flash off with pressurized steam
  - Increased volatile losses w/increasing pressure
  - Environmental impacts for VOCs



# Other Disadvantages

- Pressure sealing
  - High Maintenance
  - Expensive



John Crane Type 32 seal, good to 225 psig



## Status of pyrolysis kinetics studies

- Not very much work has been done on the effects of pressure on pyrolysis kinetics
- Much more has been done on the effect of pressure on combustion kinetics
- A review of the effect of pressure on combustion kinetics can help understand what the potential impact is on pyrolysis kinetics
- More research and work on pyrolysis kinetics is warranted, and some of it will be starting soon.



# New tools to study problem

- New Dimensionless numbers
  - Old tools included Reynolds number, Froude number, Prandtl number, Schmidt number
  - New tools include numbers which provide dimensionless correlations of the relative effects of heat transfer and reaction kinetics
    - Some of these are: Prater Number, Biot Number, Weisz Modulus, Thiele Modulus, and Effectiveness Factor
  - Newest CFD software combines particle gas phase fluid mechanics with reaction kinetics

# Biomass Characteristics

- Anisotropic
  - Affects combustion, pyrolysis and modeling parameters

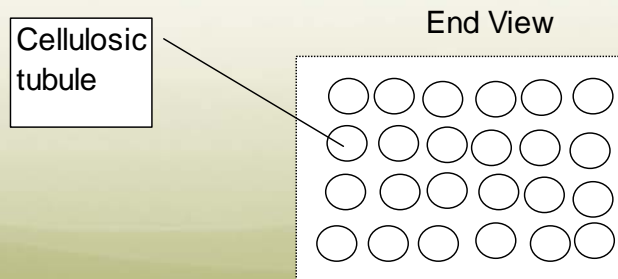
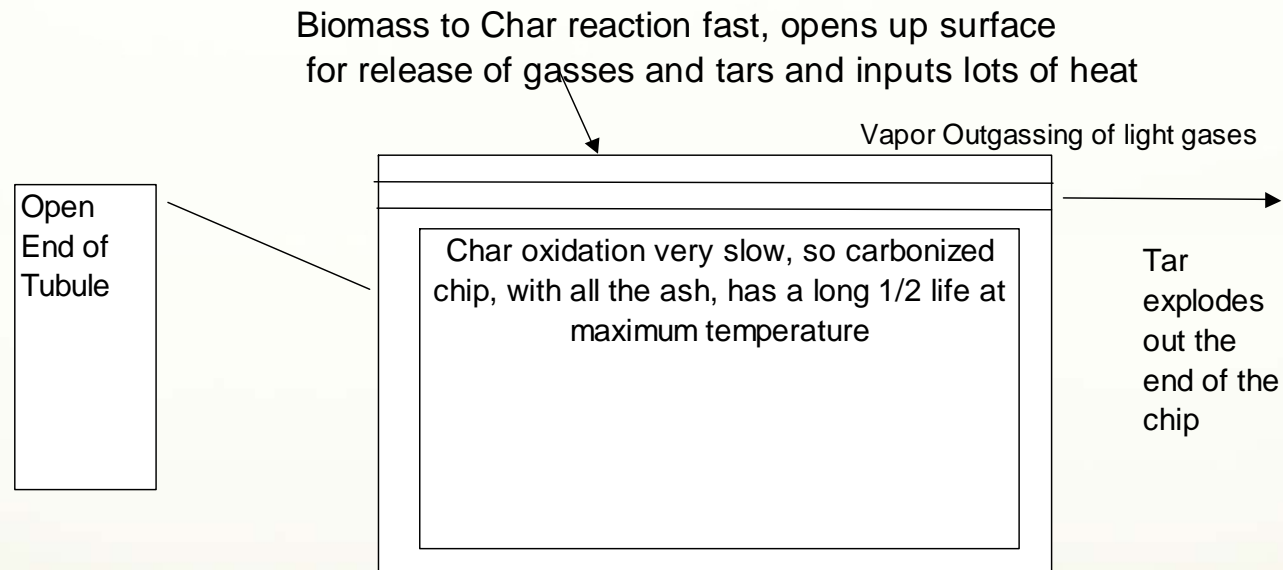




# Wood Combustion Model

## Wood Chip Undergoing Combustion

### Side View of chip







# Fireside Chat

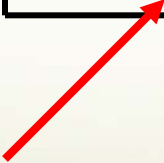
- This winter watch a fire in a fireplace for an education in combustion and pyrolysis kinetics.
- The orange flames in the fireplace are closer to pyrolysis temperatures than combustion temperatures. The cracking and popping are vapors exploding out of tubules.
- Watch a wood chip with an open end - when heated - releases a long yellow flame of tar-laden, yellow flame.
- Or get an oxy-acetylene torch, and just turn on the acetylene, then slowly turn on the oxygen.
- The smoky yellow flame will turn bright white, then get blue translucent as the incandescent carbon combusts.



# Combustion Kinetics

Reaction	Reaction Rate Constant k (1/s)
biomass--> light gas	14,400
biomass--> tar	4,130,000
biomass--> char	738,000
char oxidation	301

Rate Limiting





## Pressure Effects on Combustion

- IAE's empirical observations:

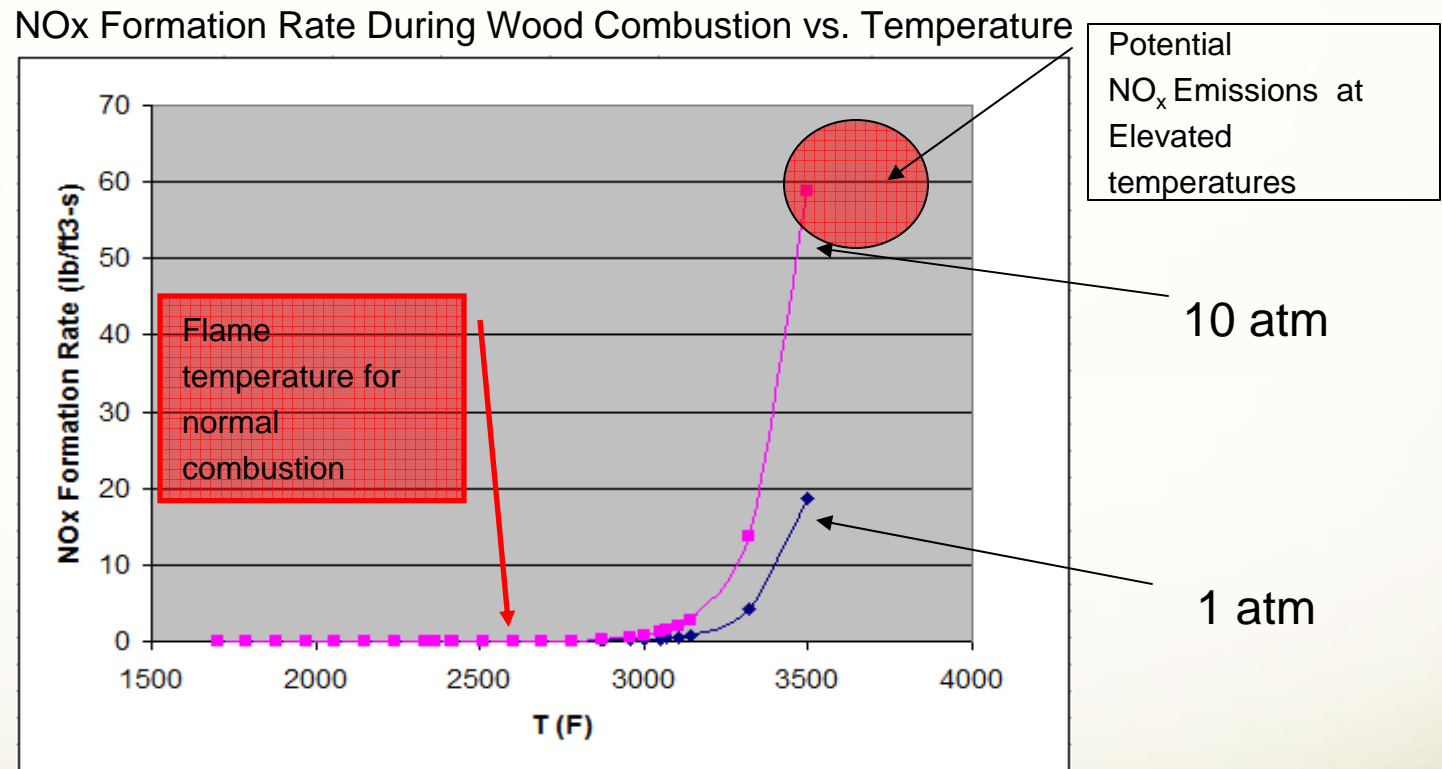
<b>Pressure</b>	<b>Flame Temperature</b>
1 atm	2500-2700 F
125-150 psig	3500-3700 F

- Results are expected
- Higher temperature indicates faster reaction rate

$$\dot{Q} = kT^4 \quad r \propto P_{O_2}^{0.5}$$



# Pressure Effects on NO<sub>x</sub> formation rates



High pressure combustion may dramatically increase NO<sub>x</sub> formation



# Pressure effect on combustion

- Published results indicate that the pressure effect on combustion kinetics is somewhat less than linear, and in some cases is close to the square root of the pressure:

- $$R = k(P_{O_2})^{0.53-0.78}$$

- Where:

- R = reaction rate
- K = constant
- $P_{O_2}$  = partial pressure of oxygen



# 1992 Gravel Bed Combustion Study

$$m_{\text{wood}} = 0.95 A_{\text{bed}} P^{0.72} T^{1.03} (\text{air/fuel})^{-0.81} (100 - \% \text{moisture})^{0.46}$$

Where the units were:

$M_{\text{wood}}$  = kg/hr

$A_{\text{bed}}$  = square meters

$P$  = atms

$T$  = degrees Kelvin

Air = kg/hr

Fuel = kg/hr

Moisture = as-received basis

“Development of a gravel bed combustor for a solid fueled gas turbine”, Ragland, et al, U of Wisconsin ME Dept., June 1992, DOE Contract No. DE-GF02-

85E40735



## Pyrolysis kinetics versus combustion kinetics

- Pyrolysis occurs at much lower temperatures than combustion
  - Half Life of wood chips is much longer than in combustion, fractions of a second instead of milliseconds
  - Thermal driving force is lower, since the temperatures are lower
- More time to “distill” off the tars
- Gas phase reactions slower, less cracking of tars, and reactions do not reach equilibrium
- No free oxygen to accelerate char oxidation



# Pyrolysis versus combustion

- Reaction rates are slower
- More tars are formed in pyrolysis
- More carbon remains in the char in pyrolysis
- Pyrolysis equipment needs to be larger for the same throughput.
- $\text{NO}_x$  emissions lower, since there is no free oxygen



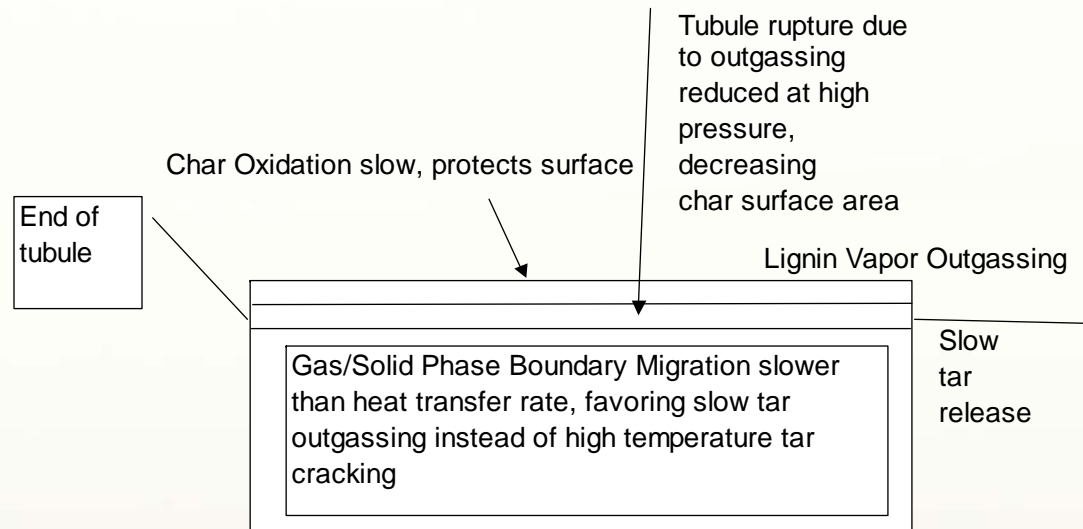


# Wood Pyrolysis Model

## Wood Chip Undergoing Pyrolysis

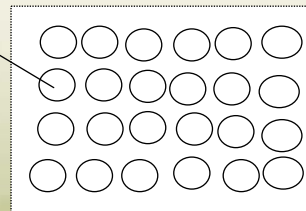
at pressure

Side View



Cellulosic tubule

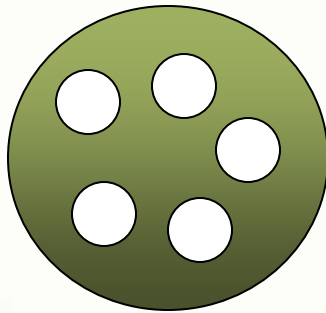
End View





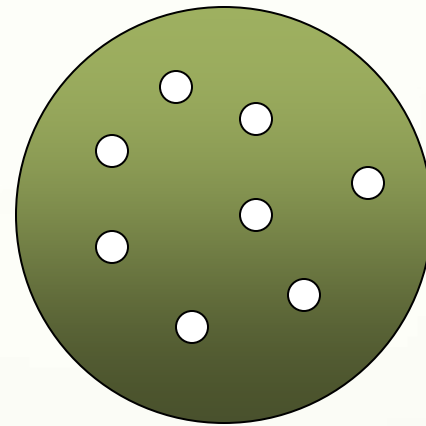
# Pyrolysis Pressure Increase Disadvantages

Low Pressure Pyrolysis Char



High pore surface area(SA)  
Smaller Particle

High Pressure Pyrolysis Char



Low pore SA: Gas diffusion  
Larger particle: Conduction

High pressure pyrolysis  $\Rightarrow$  slower char reactivity



## Potential Equipment Volume Reduction Possible

Reactor: Assume operating pressure of 300 psia, versus 1 atm.

Volume reduction due to pressure change 95%

Assume reaction rate increase is  $20^{0.6} = 6$  x more!

Total volume change  $20 \times 6 = 120$

$1/120 = 0.8\%$ . Volume of the reactor < 1% that at 1 atm.

Piping : diameter reduction due to volume decrease~  $(300/15)^{0.5} = 4.5$ ; assume pipe dia. req.  $\frac{1}{4}$  the 1 atm. Case

Footprint Reduction: Unfortunately, as yet.....to be determined



# Pyrolysis & Combustion Kinetics Theory

## Pyrolysis Kinetics

- Not well understood area
  - Equilibrium unknown as a function of time; product gases not at equilibrium
  - Prediction of product gas composition and reactor sizing needs development
- Ongoing research on pressurized pyrolysis: Georgia Tech – pyrolysis research in operational 80 atm reactor funded by DOE( NREL).

## Combustion Kinetics

- Some good data available, understanding of the full implications still have a fundamental problem with the measurement and prediction of kinetic rate equations at high pressure and temperature
- $\text{NO}_x$  formation rates at high pressure problematic.



# Conclusions

## Pressurization Advantages:

- Eliminates downstream pressurization capital and operating costs (compressors)
- Huge Capital cost reduction with equipment size reduction due to pressure and faster kinetics
- Latent Heat recovery at higher temperatures

## Disadvantages:

- Pressurized feed system
- Decreased char reactivity
- Not well understood effect on reaction rate
- Expensive pressure sealing, particularly with respect to hydrogen.

**Conclusion: Benefits of pressurization still outweigh negative impacts; further research is still desperately needed**